1,	A student is required t in the social sciences. The word closest in ma	eaning to comprehension	<u>n</u> is	of the sul	bject, especially
Anem	(A) understanding er: (A)	(B) meaning	(C) concer	otration	(D) stability
Ausw	Cr. (A)				
2.	sentence. One of his biggest	opriate word from the was his ability	to forgive.		
		(B) virtues	(C) choices	(D) s	rength
Answ	er: (B)				
3.	Which one of the statements? (A) Rajan has decided (B) Rajan and Sajan w (C) Sajan had decided	plained to Rajan that he tements below is logic to work only in a group ere formed into a group to give in to Rajan's re	preferred to work ind ally valid and can be a. against their wishes, quest to work with hir	lependently e inferred n.	100
Anew	(D) Rajan had believed er: (D)	I that Sajan and he wou	id be working togethe	Ľ.	
ZYUSW	CA. (1.0)	0	0		
4.	If y = 5x ² + 3, then the (A) passes through x = (C) is parallel to the x- er; (C)	0, y = 0	(B) has a slope of (D) has a slope of		
delining a	dv				
Ехр	er: (C) $y = 5x^2 + 3$, $\frac{dy}{dx} = 10x$ Slope of tangent = $\left(\frac{d}{d}\right)$ Slope = 0 \Rightarrow tangent is	Contract Park			
5.	A foundry has a fixed 800Q, where Q is the tonne for a daily produ	daily production in to			
Answ	er: 1300 to 1300	cuon or 100 tonness			
Exp:	Fixed cost = Rs. 50,00 Variable cost = Rs. 80 Q = daily production in For 100 tonnes of prod = 50,000+800×100 = 1	n tones nection daily, total cost 130,000	Michig		
	So, cost of production	per tonne of daily prod	uction = $\frac{130,000}{100}$ = Rs	1300.	

(C) ITZDF

(D) OYEIK

Answer: (D)

ALRVX-only one vowel EXP

EPVZB-only one vowel

FEZDF →only one vowel

OYEIK-three vowels

7. Anuj, Bhola, Chandan, Dilip, Eswar and Faisal live on different floors in a six-storeyed building (the ground floor is numbered 1, the floor above it 2, and so on). Anul lives on an even-numbered floor. Bhola does not live on an odd numbered floor. Chandan does not live on any of the floors below Faisal's floor. Dilip does not live on floor number 2, Eswar does not live on a floor immediately above or immediately below Bhola, Faisal lives three floors above Dilip. Which of the following floor-person combinations is correct?

	Anuj	Bhola	Chandan	Dilip	Eswar	Faisal
(A)	- 6	2	5	1	3	4
(B)	2	6	5	4	3	4
(C)	4	2	6	3	1	5
(D)	2	4	6	1	3	5

Answer: (E)

Exp: (a) Anuj: Even numbered floor (2.4.6)

(b) Bhola: Even numbered floor (2.4,6)

(c) Chandan lives on the floor above that of Faisal.

(d) Dilip: not on 2nd floor

(e) Eswar: does not live immediately above or immediately below Bhola From the options its clear, that only option (B) satisfies condition (e). So, correct Ans is (B).

8. The smallest angle of a triangle is equal to two thirds of the smallest angle of a quadrilateral. The ratio between the angles of the quadrilateral is 3:4:5:6. The largest angle of the triangle is twice its smallest angle. What is the sum, in degrees, of the second largest angle of the triangle and the largest angle of the quadrilateral?

Answer: 180 to 180

Expo Let the angles of quadrilateral are 3x, 4x, 5x, 6x

So, 3x+4x+5x+6x = 360

x = 20

Smallest angle of quadrilateral = 3×20 = 60°

Smallest angle of triangle = $\frac{2}{3} \times 60^{\circ} = 40^{\circ}$

Largest angle of triangle = $2 \times 40^{\circ} = 60^{\circ}$

Three angles of triangle are 40°, 60°, 80°

Largest angle of quadrilateral is 120°

Sum (2nd largest angle of triangle + largest angle of quadrilateral)

= 60°+120°=180°.

One percent of the people of country Y are taller than 6 ft. There are thrice as many people in country X as in country Y. Taking both countries together, what is the percentage of people taller than 6 ft?
 (A) 3.0
 (B) 2.5
 (C) 1.5
 (D) 1.25

Answer: (D)

Exp: Let number of people in country y = 100

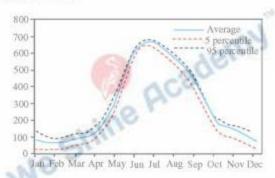
So, number of people in country x = 300

Total number of people taller than 6ft in both the countries

$$=300 \times \frac{1}{100} + 100 \times \frac{2}{100} = 5$$

% of people taller than 6ft in both the countries = $\frac{5}{400} \times 100 = 1.25\%$.

 The monthly rainfall chart based on 50 years of rainfall in Agra is shown in the following: figure. Which of the following are true? (k percentile is the value such that k percent of the data fall below that value)



- (i) On average, it mins more in July than in December
- (ii) Every year, the amount of rainfall in August is more than that in January
- (iii) July rainfall can be estimated with better confidence than February rainfall.
- (iv) In August, there is at least 500 mm of rainfall

(A) (i) and (ii) (B) (i) ar

(B) (i) and (iii) (C) (ii) and (iii)

(D) (iii) and (iv)

Answer: (B)

Exp: In the question the monthly average rainfall chart for 50 years has been given.

Let us check the options.

- (i) On average, it rains more in July than in December -> correct.
- (ii) Every year, the amount of rainfall in August is more than that in January. may not be correct because average rainfall is given in the question.
- (iii) July rainfall can be estimated with better confidence than February rainfall. ⇒ From chart it is clear the gap between 5 percentile and 95 percentile from average is higher in February than that in July ⇒ correct.
- (iv) In August at least 500 mm rainfall

So correct option (B) (i) and (iii).

⇒ May not be correct, because its 50 year average.

L Gradient of a scalar variable is always

(A) a vector

(B) a scalar

(C) a dot product

(D) zero

Answer: (A)

Gradient $\nabla = \hat{i} \frac{\partial}{\partial x} + \hat{j} \frac{\partial}{\partial y} + \hat{k} \frac{\partial}{\partial z}$ Exp.

If f is a scalar point function

$$\nabla \mathbf{f} = \operatorname{grad} \mathbf{f} = \hat{\mathbf{i}} \frac{\partial \mathbf{f}}{\partial x} + \hat{\mathbf{j}} \frac{\partial \mathbf{f}}{\partial y} + \hat{\mathbf{k}} \frac{\partial \mathbf{f}}{\partial z}$$
 is a vector.

For the time domain function, $f(t) = t^2$, which ONE of the following is the Laplace transform 2. of |f(t)dt?

(A) $\frac{3}{s^4}$ (B) $\frac{1}{4s^2}$ (C) $\frac{2}{s^3}$ (D) $\frac{2}{s^4}$ Answer: (D)

Exp. We have $L\left[\int_0^s f(t)dt\right] = \frac{F(s)}{s}$ where F(s) = L[f(t)] $\Rightarrow L\left[\int_{s}^{s} t^{2} dt\right] = \left(\frac{2}{s^{3}}\right)/3 = \frac{2}{s^{4}}\left(\sqrt{t}\left[1^{3}\right] = \frac{2}{s^{2}}\right)$

If $f^*(x)$ is the complex conjugate of $f(x) = \cos(x) + i \sin(x)$, then for real a and b, 3. $\int f^*(x)f(x)dx$ is ALWAYS

- (A) positive
- (B) negative (C) real
- (D) imaginary

Answer: (C)

Exp. f(x) = cos(x) + i sin(x) $f \cdot (x) = \cos(x) - i\sin(x)$

$$\int_{\mathbf{f}} \mathbf{f}^*(x).f(x)dx = \int_{\mathbf{f}} (\cos x - i\sin x)(\cos + i\sin x)dx$$

$$= \int e^{-ix} \cdot e^{ix} dx = \int 1 dx = b - a \in \mathbb{R} \ (\because a, b, \in \mathbb{R})$$

⇒Real for real a & b.

4. If f(x) is a real and continuous function of x, the Taylor series expansion of f(x) about its minima will NEVER have a term containing

(A) first derivative (C) third derivative (B) second derivative (D) any higher derivative Exp. For a real valued function y = I(x)

Taylor series expansion about 'a'

$$f(x)=f(a)+(x-a)f'(a)+\frac{(x-a)^2}{2!}f''(a)+...$$

For minima at x = a, f'(a) = 0.

So, Taylor series expansion of f(x) about 'a' will never contain first derivative term.

- From the following list, identify the properties which are equal in both vapour and liquid phases at equilibrium
 P. Density
 Temperature
 - R. Chemical potential
- S. Enthalpy

(A) P and Q only

(C) R and S only

(B) Q and R only (D) P and S only

Answer: (B)

Exp. For phase equilibrium

Temperature;
$$T^g = T^l$$

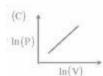
Pressure; $P^{ij} = P^{ij}$ correct Ans is (B).

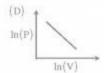
Chemical potential; $\mu^g = \mu^1$

 In a closed system, the isentropic expansion of an ideal gas with constant specific heats is represented by









Answer: (D)

Exp. For isentropic expansion,

Taking log on both sides

$$\ln P + \gamma \ln V = 0$$

$$\frac{\ln P}{\ln V} = -\gamma = \text{negative}$$

∵ y is positive slope of InP vs In V is negative.

Match the following:

Group 1	Group 2
$(P) \left(\frac{\partial G}{\partial n_i} \right)_{T,E;r_{pp}}$	I. Arrhenius equagtion
(Q) $\left(\frac{\partial \mathbf{G}}{\partial \mathbf{n}_{i}}\right)_{\mathbf{x}_{i},\mathbf{x}_{j\mu}}$	II. Reaction equilibrium constant
(R) $\exp\left(\frac{-\Delta G_{maxton}^{0}}{RT}\right)$	III. Chemical potential
(S) $\Sigma (n_i d\mu_i)_{\tau,p} = 0$	IV. Gibbs-Duhem equation
ALDERS AND SECURE CONTRACTORS	

- (A) Q-III, R-I, S-II
- (C) P-III, R-II, S-IV

(B) Q-III, R-II, S-IV
(D) P-III, R-IV, S-I

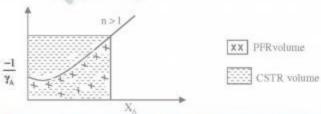
Answer: (C)

- In order to achieve the same conversion under identical reaction conditions and feed flow rate for a non-autocatalytic reaction of positive order, the volume of an ideal CSTR is
 - (A) always greater than that of an ideal PFR
 - (B) always smaller than that of an ideal PFR
 - (C) same as that of an ideal PFR
 - (D) smaller than that of an ideal PFR only for first order reaction

Answer: (A)

exp: For CSTR, volume V = PAX

For PFR volume V = F



From plot it is clear that volume of ideal CSTR (area) is higher than that of the ideal PFR.

- 9. Integral of the time-weighted absolute error (ITAE) is expressed as
 - (A) $\int_{1}^{\infty} \frac{|\varepsilon(t)|}{t^2}$

(B) $\int_{-1}^{\infty} \frac{|\varepsilon(t)|}{t} dt$

(C) $\int t |\varepsilon(t)| dt$

(D) $\int t^2 |\varepsilon(t)| dt$

Let number of people in country y = 100

So, number of people in country x = 300

Total number of people taller than 6ft in both the countries = $300 \times \frac{1}{100} + 100 \times \frac{2}{100} = 5$

% of people taller than 6ft in both the countries $=\frac{5}{3100} \times 100 = 1.25\%$

A unit IMPULSE response of a first order system with time constant rand steady state gain K_p is given by

(A)
$$\frac{1}{K_a \tau} e^{i/\tau}$$

(B) $K_{p}e^{-t/\tau}$ (C) $\tau K_{p}e^{-t/\tau}$ (D) $\frac{K_{p}}{\tau}e^{-t/\tau}$

Answer: (D)

Unit Impulse input $x(t) = \delta(t)$ Exp.

So, X(s) = 1

$$\mathbf{G}(s) \!=\! \frac{Y(s)}{X(s)} \!=\! \frac{K_p}{\tau s + 1} \Rightarrow \! y(s) \! =\! \frac{K_p}{\tau s + 1}.$$

$$y(t) = \frac{K_y}{\tau} e^{-\phi \tau}$$

demy In a completely opaque medium, if 50% of the incident monochromatic radiation is absorbed, 11. then which of the following statements are CORRECT?

(P) 50% of the incident radiation is reflected

(Q) 25% of the incident radiation is reflected

(R) 25% of the incident radiation is transmitted

(S) No incident radiation is transmitted

(A) P and S only (B) Q and R only

(C) P and Q only

(D) R and S only

Answer: (A)

For a completely opaque system $\tau = 0 \Longrightarrow S$ Exp.

Given $\infty = 0.5$

 $\infty + \tau + \gamma = 1$

So, $\gamma = 0.5 \Rightarrow P$

Final Ans is (A) P and S only.

12. In case of a pressure driven laminar flow of a Newtonian fluid of viscosity (u) through a horizontal circular pipe, the velocity of the fluid is proportional to

(B)
$$\mu^{0.1}$$

Answer: (C)

Pressure drop in case laminar flow is Exp.

$$\frac{\Delta P}{L} = \frac{32\mu LV}{D^3}$$
clearly $V = \mu^{-1}$.

- Which of the following stratements are CORRECE?
 (P) For a rheopectic fluid, the apparent viscosity increases with time under a constant applied shear stress
 - (Q) For a pseudoplastic fluid, the apparent viscosity decreases with time under a constant applied shear stress
 (R) For a Bingham plastic, the apparent viscosity increases exponentially with the
 - deformation rate
 (S) For a dilutant fluid, the apparent viscosity increases with increasing deformation rate
 - (S) For a dilatant fluid, the apparent viscosity increases with increasing deformation rate

 (A) P and Q only

 (B) Q and R only

 (C) R and S only

 (D) P and S only
- Answer: (D)
- 14. Assume that an ordinary mercury-in-glass thermometer follows first order dynamics with a time constant of 10s. It is at a steady state temperature of 0°C. At time t = 0, the thermometer is suddenly immersed in a constant temperature bath at 100°C. The time required (in s) for the thermometer to read 95°C, approximately is

(C) 30

Academy

(D) 20

(A) 60 Answer: (C)

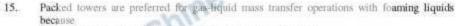
Exp. Given \u00au = 10s

For first order system

$$y(t) = K_p A(1 - e^{-\psi \tau})$$

 $95 = 100(1 - e^{-\psi \tau})$

$$\Rightarrow \frac{1}{e} = 2.995 - 3 \Rightarrow t = 30 \text{ sec.}$$



- (A) in packed towers, high liquid to gas ratios are best handled
- (B) in packed towers, continuous contact of gas and liquid takes place
- (C) packed towers are packed with random packings

(B) 40

(D) in packed towers, the gas is not bubbled through the liquid pool

Answer: (D)

- 16. A spherical storage vessel is quarter-filled with toluene. The diameter of the vent at the top of the vessel is 1/20th of the diameter of the vessel. Under the steady state condition, the diffusive flux of toluene is maximum at
 - (A) the surface of the liquid
 - (B) the mid-plane of the vessel
 - (C) the vent
 - (D) a distance 20 times the diameter of the vent away from the vent

Answer: (C)

Exp. Diffusive flux is maximum at the vent and remains same throughout the vent line at steady state.

 In order to produce fine solid particles between 5 and 10 μm, the appropriate size reducing equipment is

(A) fluid energy mill(C) jaw crusher

(B) hammer mill

(D) smooth roll crusher

absorption of controlled by (A) gas phase (C) both gas at Answer: (A) 20. Which ONE of (A) Mass trans (B) Mass trans (C) Contact tit (D) Mass trans (D) Mass trans (E) Contact tit (D) Mass trans (E) City Contact tit (E) Kilogram of (E) Kilogr		(B) diaphragm pump (D) gear pump
Answer: (B) 19. Assuming the absorption of controlled by (A) gas phase (C) both gas a Answer: (A) 20. Which ONE o (A) Mass trans (B) Mass trans (C) Contact tii (D) Mass trans (C) Contact tii (D) Mass trans (B) Kilogram (C) K	ump	(D) gear pump
19. Assuming the absorption of controlled by (A) gas phase (C) both gas a Answer: (A) 20. Which ONE of (A) Mass trans (B) Mass trans (C) Contact time (D) Mass trans (D) Mass trans (B) Mass trans (C) Contact time (D) Mass trans (D) Mass trans (D) Mass trans (E) (E) Kilogram (C)		
absorption of controlled by (A) gas phase (C) both gas at Answer: (A) 20. Which ONE of (A) Mass trans (B) Mass trans (C) Contact tin (D) Mass trans (D) Mass trans (E) Contact tin (E) Con		
Answer: (A) 20. Which ONE of (A) Mass trans (B) Mass trans (C) Contact tis (D) Mass trans (B) 21. Steam economic (A) kilogram of (B) kilogram of (C) kilogram of (D) kilogram first effect	CO ₂ from reformer g	cients in the gas and the liquid phases are comparable, the gas (CO ₂ +H ₂) into an aqueous solution of diethanolamine is (B) liquid phase resistance
Answer: (A) 20. Which ONE of (A) Mass trans (B) Mass trans (C) Contact tis (D) Mass trans (B) 21. Steam economic (A) kilogram of (B) kilogram of (C) kilogram of (D) kilogram first effect		tances (D) composition of the reformer gas.
(A) Mass trans (B) Mass trans (C) Contact tir (D) Mass trans Answer: (B) 21. Steam econom (A) kilogram of (B) kilogram of (C) kilogram of (D) kilogram first effect	S 150	
Answer: (B) 21. Steam econom (A) kilogram o (B) kilogram o (C) kilogram o (D) kilogram first effect	of the following states sfer takes place at ste sfer takes place at un me is same for all the sfer depends only on	steady state Liquid elements
(A) kilogram o (B) kilogram o (C) kilogram o (D) kilogram first effect	mer negrone only to	
(A) kilogram o (B) kilogram o (C) kilogram o (D) kilogram first effect		
Answer: (D)	of steam used per ho of steam consumed in of steam used in all th	
		a ka
	5.0	V6 ,
(A) η _D = (gra (B) η _D = (gra (C) η _D = (gra (D) η _D = (theo	ams of NaOH produc ons of NaOH produc om equivalents of Na	in electrolytic cell used for producing NaOH is defined as ed / grams of NaCl decomposed) x 100 ed / grams of NaCl charged) x 100 OH produced / gram equivalents of NaCl charged) x 100 oduce one gram equivalent / actual current to produce one
Answer: (C)		
23. The vessel dis	spersion number for a (B) 0	an ideal CSTR is (C) 1 (D) ∞
Answer: (D)		
	D	
Exp. Dispersion no		
For an ideal C	$STR, \frac{D}{UL} \rightarrow \infty$	

Catalytic cracking is
(A) a hydrogen addition process
(C) an exothermic process

24.

(B) a carbon rejection process (D) a coking process

- Which ONE of the following statements is CORRECT?" 25.
 - (A) The major components of biodiesel are triglycerides
 - (B) Biodiesel is essentially a mixture of ethyl esters
 - (C) Biodiesel is highly aromatic (D) Biodiesel has a very low aniline point

Answer: (B)

O.No-26-55 Carry Two Marks Each

Consider the following differential equation 26.

$$\frac{dy}{dx} = x + \ln(y); y = 2 \text{ at } x = 0$$

The solution of this equation at x = 0.4 using Euler method with a step size of h = 0.2 is

Answer: 2.3 to 2.4

Exp. $\frac{dy}{dx} = x + \ell ny$

$$\begin{aligned} &\frac{d\mathbf{y}}{d\mathbf{x}} = f(x,y) \implies f(x,y) = x + \ell n y \\ &\mathbf{given} \ x_0 = 0, y_0 = 2 \\ &\mathbf{We} \ have, \ y_{n+1} = y_n + h_\ell(x_n, y_n) \ n = 0.1.2, 3, \\ &\mathbf{for} \ x = 0 \ y_1 = y_0 + h_\ell(x_0, y_0) \\ &\mathbf{h} = 0.2, \ y_1 = y(x_1) = y(x_0 + h) = y(0 = 0.2) = y(0.2) \end{aligned}$$

We have,
$$y_{n+1} = y_n + h_1(x_n, y_n) = 0.1, 2, 3,...$$

for
$$x = 0$$
 $y_1 = y_0 + h_1(x_0, y_0)$

$$h=0.2$$
, $y_1=y(x_1)=y(x_0+h)=y(0+0.2)=y(0.2)$

$$x, y(0.2) = y_1 = 2 + 0.2 f(0.2) = 2 + 0.2 (0 + ln_y) = 2 + 0.2 (0.69315) = 2.13863$$

$$y_1 = y(x_1) = y(x_1+h) = y(0.2+0.2) = y(0.4)$$

$$y(0.4) = y_1 = y_2 + b_1(x_1, y_1) = 2.13863 + 0.2f(0.2, 2.13863)$$

The integrating factor for the differential equation 27.

$$\frac{dy}{dx} - \frac{y}{1+x} = (1+x)$$
 is

$$dx = 1 + x$$

A)
$$\frac{1}{1+x}$$

(A)
$$\frac{1}{1+x}$$
 (B) $(1+x)$ (C) $x(1+x)$ (D) $\frac{x}{1+x}$

Answer: (A)

Given differential equation $\frac{dy}{dx} - \frac{y}{1+x} = 1+x$ Exp.

$$\frac{dy}{dx} + Py = Q \Rightarrow P = \frac{-1}{1+x}$$

LF =
$$e^{\int_{0.0}^{\infty}} = e^{\int_{1+x}^{-L} dx} = e^{-i\omega(1+x)} = \frac{1}{1+x}$$

- 28. The differential equation $\frac{d^2y}{dx^2} + x^2 \frac{dy}{dx} + x^2y = e^x$ is a
 - (A) non-linear differential equation of first degree
 - (B) linear differential equation of first degree
 (C) linear differential equation of second degree
 - (D) non-linear differential equation of second degree

Answer: (B)

Exp. Given equation

$$\frac{d^2y}{dx^2} + x^3 \frac{dy}{dx} + x^2y = e^x$$

This is clearly a linear differential equation

Order = 2

Degree = 1.

29. Consider the following two normal distributions

$$\mathbf{f}_{t}(\mathbf{x}) = \exp(-\pi \mathbf{x}^{2})$$

$$f_{a}(x) = \frac{1}{2\pi} \exp \left\{ -\frac{1}{4\pi} (x^{2} + 2x + 1) \right\}$$

If μ and σ denote the mean and standard deviation, respectively, then

(A) $\mu_1 < \mu_2$ and $\sigma_1^2 < \sigma_2^2$

(B) $\mu_1 < \mu_2$ and $\sigma_1^2 > \sigma$

(C) $\mu_1 > \mu_2$ and $\sigma_1^2 < \sigma_2^2$

(D) $\mu_1 > \mu_2$ and $\sigma_1^2 > \sigma_2$

Answer: (C)

Exp. $f_1(x) = e^{-\alpha x^2}$

Comparing with,
$$f(x) = \frac{1}{\sigma \sqrt{2\pi}} e^{-\frac{1}{\alpha}} \left(\frac{x - \mu}{\sigma}\right)^2$$

$$\Rightarrow \mu_1 = 0 \& \sigma_1 = \frac{1}{\sqrt{2\pi}}$$

$$f_2(x) = \frac{1}{2\pi} e^{\frac{1}{4\pi}(x^2 + 2\pi xt)} = \frac{1}{2\pi} e^{\frac{1}{4\pi}(x+t)^2}$$

Comparing with ,
$$f(x) = \frac{1}{\sigma \sqrt{2\pi}} e^{-\frac{1}{2} \left(\frac{x-\mu}{\sigma}\right)}$$

$$\Rightarrow \mu = -1 \& \sigma_1 = \sqrt{2\pi}$$

$$\Rightarrow \mu_1 > \mu_2 \& \sigma_1^2 < \sigma_2^2 \Rightarrow (C)$$

 In rolling of two fair dice, the outcome of an experiment is considered to be the sum of the numbers appearing on the dice. The probability is highest for the outcome of

Answer: 6.99 to 7.01

Exp.

X 2 3 4 5 6 7 8 9 10 11 12

P(x)		6 36	36	36	36	36	36	36	2 36	1 36
------	--	------	----	----	----	----	----	----	---------	------

Where X is a random variable denotes the sum of the numbers appearing on the dice.

P(x) = corresponding probabilities

. The probability is highest for the outcome "7" i.e.,
$$\frac{6}{36}$$

- 31... A spherical ball of benzoic acid (diameter = 1.5 cm) is submerged in a pool of still water. The solubility and diffusivity of benzoic acid in water are 0.03 kmol/m and 1.25 x 109 m2/s respectively. Sherwood number is given as Sh = 2.0 + 0.6 Re 13 Sc 133. The initial rate of dissolution (in kmol/s) of benzoic acid approximately is
 - (A) 3.54×10⁻¹¹

(B) 3.54×10⁻¹²

(C) 3.54×10⁻¹³

(D) 3.54×10⁻¹⁸

Answer: (B)

Exp.
$$Sh = 2 + 0.6 R_{\odot}^{0.5} Se^{0.37}$$

Diameter = 1.5 cm

Solubility = 0.03 k mol/m

Given
$$Sh = 2 + 0.6(Re)^{0.5} (Sc)^{0.5}$$

Initially Sh-2

Diameter = 1.5 cm
Solubility =
$$0.03 \text{ k mol/m}^3$$

Diffusivity = $1.25 \times 10^{-8} \text{ m}^3/\text{s}$
Given Sh = $2 \div 0.6 (\text{Re})^{0.5} (\text{Se})^{0.5}$
Initially Sh - 2
 $\frac{\text{K}_s d}{\text{D}_{4.9}} = 2$, $\text{K}_s = \text{Mass transfer coefficient (m/s)}$

$$\Rightarrow$$
 K, = $\frac{2 \times 1.25 \times 10^{-7}}{1.5 \times 10^{-7}}$ = 1.67 × 10⁻⁷ m/sec

Initial rate of dissolution = $K_A(C_1 - 0) = K_0AC_1$

=1.67×10⁻¹×
$$\pi$$
×(1.5×10⁻¹)²×0.03=3.54×10⁻¹² kmol/sec

32. A wet solid of 100 kg is dried from a moisture content of 40wt% to 10wt%. The critical moisture content is 15wt% and the equilibrium moisture content is negligible. All moisture contents are on dry basis. The falling rate is considered to be linear. It takes 5 hours to dry the material in the constant rate period. The duration (in hours) of the falling rate period is

Answer: 1.1 to 1.3

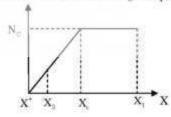
Exp. Given $X_1 = 0.4$

$$X_2 = 0.10$$

$$X_{\rm C} = 0.15$$

$$X^* = 0$$

Constant rate period



$$5 = \frac{S}{AN_c} (X_1 - X_c) \Rightarrow \frac{S}{AN_c} = \frac{S}{0.25} = 20$$

Falling rate period, $N = m(X - X^*) = \frac{N_c(X - X^*)}{(X_c - X^*)}$

$$t_{e} = -\int\limits_{X_{e}}^{X_{e}} \frac{S}{A} \frac{dX}{\left(\frac{N_{e}}{X_{e} - X^{*}}\right) (X - X^{*})} = \frac{S(X_{e} - X^{*})}{AN_{e}} \ln \frac{X_{e} - X^{*}}{X_{e} - X^{*}}$$

$$t_t = 20 \times 0.15 \ln \frac{0.15}{0.10} = 1.216 \text{ hr.}$$

33. A brick wall of 20 cm thickness has thermal conductivity of 0.7 W m⁻¹ K⁻¹. An insulation of thermal conductivity 0.2 W m⁻¹ K⁻¹ is to be applied on one side of the wall, so that the heat transfer through the wall is reduced by 75%. The same temperature difference is maintained across the wall before and after applying the insulation. The required thickness (in cm) of the insulation is

Answer: 17.0 to 17.3

Exp. Before insulation heat flux

$$\mathbf{Q}_1 = -\mathbf{k}_1 \mathbf{A} \frac{\mathbf{d} \mathbf{T}^2}{\mathbf{d} \mathbf{x}_1} = -\mathbf{k}_1 \mathbf{A} \frac{\mathbf{\Delta} \mathbf{T}}{0.2}$$

After applying insulation heat transfer decreases by 75%

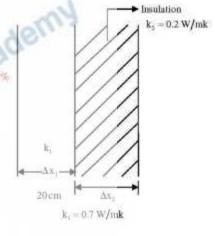
$$Q_2 = -\frac{\Delta T}{\frac{\Delta x_1}{k_1 \Delta} + \frac{\Delta x_2}{k_2 \Delta}}$$

Taking A = 1m

$$Q_2 = 0.25 Q_1 = 0.25 \frac{\Delta T}{0.2} = \frac{\Delta T}{0.2} = \frac{\Delta T}{0.7} = \frac{\Delta T}{0.7} = \frac{\Delta T}{0.7} = \frac{\Delta T}{0.2} = \frac{\Delta T}{0.7} = \frac{\Delta T}{0.2} = \frac{\Delta T}$$

$$\Rightarrow \frac{0.8}{0.7} = \frac{0.2}{0.7} + \frac{\Delta x_1}{0.2}$$

$$\Rightarrow \Delta x_2 = \frac{0.6 \times 0.2}{0.7} = 0.1714 \text{m} = 17.14 \text{ cm}.$$



34. An oil with a flow rate of 1000 kg/h is to be cooled using water in a double-pipe counter-flow heat exchanger from a temperature of 70°C to 40°C. Water enters the exchanger at 25°C and leaves at 40°C. The specific heats of oil and water are 2 kJ kg ¹ K ¹ and 4.2 kJ kg ¹ K ¹, respectively. The overall heat transfer coefficient is 0.2 kW m ³ K ¹. The minimum heat exchanger area (in m ³) required for this operation is

Answer: 3,75 to 3.95

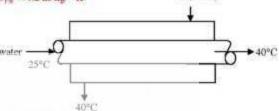
Given
$$C_{po} = 2 \text{ kJ kg}^{-1} \text{K}^{-1}$$
 $C_{pw} = 4.2 \text{ kJ kg}^{-1} \text{ K}^{-1}$

$$C_{PN} = 4.2 \text{ kJ}$$

$$U = 0.2 \text{ kW m}^{-2} \text{K}^{-1}$$

$$\Delta T_1 = 15^{\circ}C$$
, $\Delta T_2 = 30^{\circ}C$

$$LMTD = \frac{30 - 15}{\ln\left(\frac{30}{15}\right)} = 21.64^{\circ}C$$



oil (70°C)

Heat transfer
$$Q = \frac{1000}{3600} \times 2 \times (70^{\circ} - 40^{\circ}) = 16.67 \text{ kJ}$$

$$\mathbf{A} = \frac{16.67}{0.2 \times 21.64} = 3.85 \,\text{m}^3$$
.

Which ONE of the following is CORRECT for an ideal gas in a closed system? 35.

(A)
$$\left(\frac{\partial U}{\partial V}\right)_{\alpha} V = nR\left(\frac{\partial U}{\partial S}\right)$$

(B)
$$-\left(\frac{\partial H}{\partial P}\right) P = nR\left(\frac{\partial H}{\partial S}\right)$$

(A)
$$\left(\frac{\partial U}{\partial V}\right)_{g} V = nR \left(\frac{\partial U}{\partial S}\right)_{g}$$
 (B) $-\left(\frac{\partial H}{\partial P}\right)_{g} P = nR \left(\frac{\partial H}{\partial S}\right)_{g}$ (C) $\left(\frac{\partial U}{\partial V}\right)_{g} V = nR \left(\frac{\partial H}{\partial S}\right)_{g}$ (D) $\left(\frac{\partial H}{\partial P}\right)_{g} P = nR \left(\frac{\partial U}{\partial S}\right)_{g}$

Answer: (D)

Exp. (A)
$$\left(\frac{\partial u}{\partial v}\right) v = nR\left(\frac{\partial u}{\partial s}\right)$$

Fundamental property relation

Fundamental property relation

dU = Tds - Pdv

$$\Rightarrow \left(\frac{\partial \mathbf{u}}{\partial \mathbf{v}}\right) = -\mathbf{P} \text{ and } \left(\frac{\partial \mathbf{u}}{\partial \mathbf{s}}\right) = \mathbf{T}$$

-PV = nRT -> Incorrect

$$\{\mathbf{B}\}$$
 $-\left(\frac{\partial H}{\partial P}\right)P = nR\left(\frac{\partial H}{\partial S}\right)$

Fundamental property relation

dH = Tds + Vdp

$$\left(\frac{\partial H}{\partial P}\right) = V \text{ and } \left(\frac{\partial H}{\partial S}\right) = T$$

$$-PV = nRT \Rightarrow incorrect$$

A binary distillation column is operating with a messal feed containing 20 mol% vapour. If 36: the feed quality is changed to 80 mol% vapour, the change in the slope of the q-line is

Answer: 3.6 to 3.9

Exp. Feed contains 20% vapour, so
$$q = 0.8$$

Slope of q line =
$$\frac{q}{q-1} = \frac{0.8}{-0.2} = -4$$

Slope =
$$\frac{q}{q-1} = \frac{0.2}{-0.8} = \frac{-1}{4}$$

Change in slope =
$$-\frac{1}{4} + 4 = 3.75$$
.

37. A homogeneous reaction $(R \to P)$ occurs in a batch reactor. The conversion of the reactant R For an ideal batch reactor $A = \int_{C_A}^{C_A} \frac{dC_A}{-Y} = \int_{C_{AB}}^{C_A} \frac{dC_A}{kC_A^n}$ $C_A = C_{AB}(1 - X_A)$ $C_A = -C_{AB}dX_A$ $= -C_A \int_{C_A}^{C_A} dX$ is 67% after 10 minutes and 80% after 20 minutes. The rate equation for this reaction is $(D) - r_R = kC_R^{0.3}$

Answer: (B)

Exp. For an ideal batch reactor
$$A = \int_{c_{ab}}^{a} \frac{dC_{a}}{-\gamma} = \int_{c_{ab}}^{a} \frac{dC_{a}}{kC_{a}}$$

$$\mathbf{C}_{A} = \mathbf{C}_{AB} (\mathbf{I} - \mathbf{X}_{A})$$

$$dC_A = -C_{AB}dX_A$$

$$t = -C_{A0} \int \frac{dX_A}{kC_{A0}^* (1-X_A)^0} = \frac{C_{A0}}{k} \int_0^\infty \frac{dX_A}{(1-X_A)^n}$$

$$t = \frac{C_{A0}^{1-n}}{k} \left[\frac{(1+X_A)^{nn}}{1-n} \right]^{X_A}$$

$$\mathbf{I} = \frac{C_{A0}^{1-\alpha}}{k} \left[\frac{(1-X_A)^{1-\alpha} - 1}{1-n} \right]$$

for reaction R
$$\rightarrow$$
 P; $X_A = 0.67$, $t = 10$ minutes

$$X_A = 0.80 t = 20 \text{ minutes}$$

$$10 = C_{x,0}^{6-n} \left[\frac{0.33^{1-n} - 1}{1-n} \right]$$
 (1)

$$20 = \frac{C_{A0}^{1-n}}{k} \left[\frac{0.2^{1-n}-1}{1-n} \right] (2)$$

Dividing equation (1) by equation (2)

$$\frac{1}{2} = \frac{0.33^{1-n} - 1}{0.2^{1-n} - 1}$$

Solving we get n=2

A vapour phase catalytic reaction [Q+R-+S] follows Rideal mechanism (R and S are not 38. adsorbed). Initially, the mixture contains only the reactants in equimolar ratio. The surface

reaction step is rate controlling. With constants a and b, the initial rate of reaction $(-r_a)$ in

terms of total pressure (PT) is given by

(A)
$$-\mathbf{r}_0 = \frac{\mathbf{a}P_T^2}{1 + \mathbf{b}P_T}$$
 (B) $-\mathbf{r}_0 = \frac{\mathbf{a}P_T^2}{1 + \mathbf{b}P_T^2}$ (C) $-\mathbf{r}_0 = \frac{\mathbf{a}P_T^2}{1 + \mathbf{b}P_T}$ (D) $-\mathbf{r}_0 = \frac{\mathbf{a}P_T^3}{1 + \mathbf{b}P_T}$

Answer (C)

Rated mechanism EXIX

$$A(g) + S \xrightarrow{E_1} A - S$$

$$A - S + B(g) \xrightarrow{E_1} AB - S$$
 (rate controlling)

$$AB-S \longrightarrow AB$$

$$\mathbf{k}_t = \frac{A - S}{(A)(S)}$$
 (1)

Here s = adsorption site on catalyst surface
$$\mathbf{k}_1 = \frac{\mathbf{A} - \mathbf{S}}{(\mathbf{A})(\mathbf{S})} \qquad (1)$$
and for rate controlling step
$$-\mathbf{y} = \mathbf{K}_2 (\mathbf{A} - \mathbf{s})(\mathbf{B}) - \mathbf{K}_2 (\mathbf{A}\mathbf{B} - \mathbf{S}) \qquad (11)$$
Also, total number of sites is \mathbf{S}_1

$$\mathbf{S}_T = (\mathbf{S}) + (\mathbf{A} - \mathbf{S}) + (\mathbf{A}\mathbf{B} - \mathbf{S}) \qquad (111)$$

$$S_T = (S) + (A - S) + (AB - S) _ (III)$$

Initially surface coverage of AB will be very low, so (AB-8)=0

From (1),
$$K_1 = \frac{(A-S)}{(A)(S_1 - (A-S))}$$

$$\Rightarrow K_1(A)S_7 - K_1(A-S)(A) = (A-S) \Rightarrow (A-S) = \frac{K_1(A)S_7}{1+K_1(A)}$$

Now, for rate controlling step, $-\gamma = K$, (A-S)(B)-K, (AB-S)

Initial rate mean concentration of (AB-S)→0

So,
$$-\gamma_0 = K_{-1}(A-S)(B)$$

$$-\gamma_0 = \frac{K_z K_z (A)(B) S_z}{1 + K_z (A)}$$

For the given reaction Q+R-S with reactants in equimolar ratio

$$-\gamma_0 = \frac{K_2 K_2 P_T P_T}{1 + K_1 P_T} = \frac{a P_T^2}{1 + b P_T}$$

39. A incompressible fluid is flowing through a contraction section of length L and has a 1-D (x direction) steady state velocity distribution, $u = u_0 \left(1 + \frac{2x}{L}\right)$. If $u_0 = 2m/s$ and L = 3m, the convective acceleration (in m/s^2) of the fluid at L is

convective acceleration (in m/s2) of the fluid at L is_

Answer: 7,99 to 8.01

Exp.

Convective acceleration
$$\frac{dt}{dt} = \frac{\partial u}{\partial t} + u \frac{dx}{dx} + \dots$$

$$= u_0 \left(1 + \frac{2x}{L} \right) \frac{2u_0}{L}$$

Putting
$$u_0 = 2, L = 3$$

at
$$x = L$$
, convective acceleration = $2\left(1 + \frac{2L}{L}\right)\left(\frac{2\times 2}{3}\right) = 8 \text{ m/s}^3$.

40. Match the following:

Group 1	Group 2	
(P) Tank in series model	(I) Non-isothermal reaction	
(Q) Liquid-liquid extraction	(II) Mixer-settler	
(R) Optimum temperature progression	(III) PFR with axial mixing	
(S) Thiele modulus	(IV) Solid catalyzed reaction	

- (A) P-II, Q-IV, R-I, S-III
- (C) P-III, O-1, R-II, S-IV

- (B) P-I, Q-II, R-III, S-IV
- (D) P-III, Q-II, R-I, S-IV

Answer: (D)

Exp. Tank in series model -> PFR with axial mixing

Liquid-liquid extraction -> Mixer settler

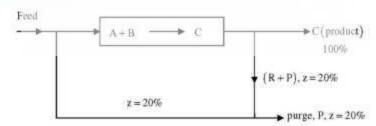
Optimum temperature progression -> Non-isothermal reaction

Thiele modulus -> Solid catalyst reaction.

41. Two elemental gases (A and B) are reacting to form a liquid (C) in a steady state process as per the reaction. A+B→C. The single-pass conversion of the reaction is only 20% and hence recycle is used. The product is separated completely in pure form. The fresh feed has 49 mol% of A and B each along with 2 mol% impurities. The maximum allowable impurities in the recycle stream is 20 mol%. The amount of purge stream (in moles) per 100 moles of the fresh feed is

Answer: 9,99 to10.01

Exp.



Basis = 100 moles of fresh feed

A = 49 moles; B = 49 moles;

lnert, z = 2 moles

Overall balance on inert

$$2 = P \times 0.2 \implies P = 10$$

42. Carbon monoxide (CO) is burnt in presence of 200% excess pure oxygen and the flame temperature achieved is 2298 K. The inlet streams are at 25 °C. The standard heat of formation (at 25 °C) of CO and CO2 are -110kJ mol and -390kJ mol respectively. The heat capacities (in J mol 1 K 1) of the components are

$$C_{p_{oc}} = 25 + 14 \times 10^{-1} \text{ T}$$

$$C_{\text{fem.}} = 25 + 42 \times 10^{-1} \text{T}$$

where, T is the temperature in K. The heat loss (in kJ) per mole of CO burnt

Answer: 32.0 to 38.0

Exp.
$$CO + \frac{1}{2}O_2 \longrightarrow CO_3$$

Basis: I mole of CO burnt

$$O_2$$
 supplied = $0.5 \times 3 = 1.5$ mole

Unreacted O₂ in product = 1 mole

cademy Standard heat of reaction = - 390 - (-110) = - 280 kJ/mol.

Heat of reactants = 0 (at 298k)

Heat of product =
$$\int_{2\pi}^{22\pi} \left\{ (25 + 1.4 \times 10^{-3} \text{T}) + (25 + 42 \times 10^{-9} \text{T}) \right\} dT$$
= 86.344 + 159.032 = 245.376 kJ/mole

43. A cash flow of Rs. 12,000 per year is received at the end of each year (uniform periodic payment) for 7 consecutive years. The rate of interest is 9% per year compounded annually. The present worth (in Rs.) of such cash flow at time zero is

Answer: 60000 to 61000

Exp. Present worth
$$P = R \left[\frac{(1+i)^n - 1}{i(1+i)^n} \right]$$

$$P = 12000 \left[\frac{(1.09)^7 - 1}{0.09 \times (1.09)^7} \right] = 60395.43$$

44. A polymer plant with a production capacity of 10,000 tons per year has an overall yield of 70%, on mass basis (kg of product per kg of raw material). The raw material costs Rs. 50,000 per ton. A process modification is proposed to increase the overall yield to 75% with an investment of Rs. 12.5 crore. In how many years can the invested amount be recovered with the additional profit?

Answer: 2.55 to 2.70

Exp. Let number of years = n

Total product = 10,000 n

Raw material used =
$$\frac{10,000 \text{ n}}{0.7}$$

Total cost of Raw material=
$$\frac{10,000 \text{ n}}{0.7} \times 50,000$$

from question

$$\frac{50,000\times10,000\,n}{0.7} = \frac{50,000\times10,000\,n}{0.75} = 12.5\times10^7$$

Solving, n = 2.625 years.

45. A step change of magnitude 2 is introduced into a system having the following transfer function:

$$G(s) = \frac{2}{s^2 + 2s + 4}$$
is
$$\frac{0.5}{5s^2 + 0.5s + 1}$$
...

The percent overshoot is

Answer: 16.0 to 16.8

Exp.
$$G(s) = \frac{2}{s^2 + 2s + 4} = \frac{0.5}{0.25s^2 + 0.5s + 1}$$

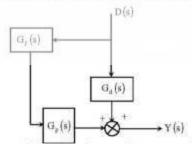
Comparing with
$$G(s) = \frac{K}{s}$$

$$p = 0.5$$
 $p = 0.5$

overshoot = exp
$$\left[-\frac{\pi \rho}{\sqrt{1 - \rho^2}} \right]$$
 = exp $\left[\frac{-\pi \times 0.5}{\sqrt{1 - 0.25}} \right]$ = 0.1630

% overshoot = 16.3%

Given below is a simplified block diagram of a feedforward control system.



The transfer function of the process is $G_p = \frac{3}{6+1}$ and the disturbance transfer function is

 $G_4 = \frac{1}{e^2 + 2e + 1}$. The transfer function of the PERFECT feed forward controller, $G_6(s)$ is

(A)
$$\frac{-5}{(s+1)^3}$$
 (B) $\frac{-5}{(s+1)}$ (C) $\frac{-1}{5(s+1)}$

(B)
$$\frac{-5}{(s+1)}$$

(C)
$$\frac{-1}{5(s+1)}$$

(D)
$$-5(s+1)$$

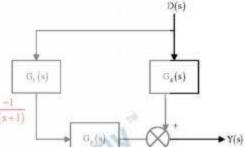
Answer: (C)

Exp.
$$\frac{\mathbf{Y}(s)}{\mathbf{D}(s)} = G_t(s) \times G_y(s) + G_z(s)$$

For perfect feed forward controller, no effect of load disturbances.

$$\Rightarrow$$
 G₁(s)×G₂(s)+G₄(s)=0

$$\Rightarrow G_{r}(s) = \frac{-G_{d}(s)}{G_{p}(s)} = \frac{-1}{(s+1)^{2} \cdot \frac{5}{s}} = \frac{-1}{5(s+1)}$$



The bottom face of a horizontal slab of thickness 6 mm is maintained at 300°C. The top face 47. is exposed to a flowing gas at 30°C. The thermal conductivity of the slab is 1.5 W m1K1 and the convective heat transfer coefficient is 30 W m 2 K 1. At steady state, the temperature (in "C) of the top face is

Answert 268 to 274

EXP.

At steady state

heat flux due to conduction = heat flux due to convection

$$\Rightarrow -kA \frac{(573 - T_s)}{6 \times 10^{-3}} = hA (T_s - 303)$$

$$\Rightarrow 1.5(573 - T_s) = 6 \times 10^{-3} \times 30 (T_s - 303)$$

$$859.5 - 1.5T_s = 0.18 T_s - 54.54$$

48. In a steady incompressible flow, the velocity distribution is given by \(\overline{V} = 3x\hat{1} - Py\hat{3} + 5z\hat{k}\), where, \(V\) is in m/s and \(x\), \(y\), and \(z\) are in m. In order to satisfy the mass conservation, the value of the constant \(P\) (in s⁴) is

Answer: 7.99 to 8.01

Exp. Given
$$\overline{V} = 3x\hat{i} - Py\hat{j} + 5z\hat{k}$$

For mass conservation at constant density

$$\Delta . \overline{V} = 0$$

$$\Rightarrow \frac{\partial V_a}{\partial x} + \frac{\partial V_y}{\partial y} + \frac{\partial V_a}{\partial z} = 0$$

$$\Rightarrow 3 - P + 5 = 0 \Rightarrow P = 8$$

49. Match the following

Group I	Group II
(P) Turbulence	(I) Reciprocating pump
(Q) NPSH	(II) Packed bed
(R) Ergun equation	(III) Fluctuating velocity
(S) Rotameter	(IV) Impeffer
(T) Power number	(V) Vena contracta

Answer: (A)

Exp. Turbulence: Characterized by fluctuating velocity.

Ergun equation: for calculating pressure drop in packed bed.

Power number: For calculating power consumption in mixing tank.

50. In a steady and incompressible flow of a fluid (density = 1.25 kg m³), the difference between stagnation and static pressures at the same location in the flow is 30 mm of mercury (density = 13600 kg m³). Considering gravitational acceleration as 10 m s², the fluid speed (in m s³) is

Answer: 79 to 82

Exp. Bernoulli's equation

$$\begin{split} &\frac{P_z}{\rho_r g} + \frac{v^2}{2g} = \frac{P}{\rho_r g} + 0 \Longrightarrow v = \sqrt{\frac{2(P - P_r)}{\rho_r}} \\ &\text{Given } \frac{P - P_g}{\rho_r} = \frac{\rho g h}{\rho_r} = \frac{13600 \times 10 \times 30 \times 10^{-3}}{1.25} = 3264 \\ &v = \sqrt{2 \times 3264} = 80.8 \text{ m/sec.} \end{split}$$

Consider a binary liquid mixture at equilibrium with its vapour at 25°C. 51.

Antoine equation for this system is given as $log_{10} p_1^{ne} = A - \frac{B}{t+C}$ where t is in ${}^{\circ}C$ and p in Torr.

The Antoine constants (A, B, and C) for the system are given in the following table.

Component	A	В	C
1	7.0	1210	230
2	6.5	1206	223

The vapour phase is assumed to be ideal and the activity coefficients (γ_i) for the non-ideal liquid phase are given by

$$\ln(\gamma_1) = x_1^2 [2 - 0.6x_1]$$

$$\ln(\gamma_2) = x_1^2 [1.7 + 0.6x_2]$$

If the mole fraction of component 1 in liquid phase (x1) is 0.11, then the mole fraction of component 1 in vapour phase (vi) is

Answer: 0.65 to 0.75

Exp.
$$log_{10} P_1^{sa} = A - \frac{B}{t+c}$$

component 1 in vapour phase (y_t) is

ver: 0.65 to 0.75

$$\log_{10} P_1^{tot} = A - \frac{B}{t+c}$$
For component 1.
$$\log_{10} P_1^{tot} = 7 - \frac{1210}{25 + 230} = 2.2549$$

$$P_1^{tot} = 179.846 \text{ Torr}$$

$$\text{and } \ln{(\gamma_t)} = x_2^3 (2 - 0.6x_0)$$

$$\text{put } x_1 = 0.41$$

$$y_1 = \exp{(0.88)^3 (2 - 0.6 \times 0.11)} = y_1 = 4.627$$

and
$$\ln(\gamma_1) = \chi_2^3 (2 - 0.6\chi)$$

put
$$x_1 = 0.17$$

$$\gamma_i = \exp[0.89^{\circ}(2 - 0.6 \times 0.11)] \Rightarrow \gamma_i = 4.627$$

For component 2,
$$\log_{10} P_2^{\text{en}} = 6.5 - \frac{1206}{25 + 223} = 1.637$$

$$P_3^{eff} = 43.36 \text{ Torr} \text{ and } \ln(\gamma_1) = x_1^2(1.7 + 0.6x_2)$$

$$\gamma_2 = \exp[0.11^2(1.7 + 0.6 \times 0.11)]$$

$$\Rightarrow \gamma_1 = 1.021598$$

From modified Raoult's law, $y_1P = x_1\gamma_1P_1^{at}$ and $y_2P = x_2\gamma_1P_1^{at}$

$$\Rightarrow y_1 = \frac{x_1 \gamma_1 P_1^{ext}}{x_1 \gamma_1 P_1^{ext} + x_2 \gamma_2 P_2^{ext}}$$

$$\Rightarrow y_1 = \frac{0.11 \times 4.627 \times 179.846}{0.11 \times 4.627 \times 179.846 + 0.89 \times 1.021598 \times 43.36}$$

$$\Rightarrow y_1 = 0.699.$$

52. A process with transfer function, $G_{ij} = \frac{2}{s-1}$ is to be controlled by a feedback proportional

controller with a gain K_c . If the transfer functions of all other elements in the control loop are unity, then which **ONE** of the following conditions produces a stable closed loop response?

(A) $K_c = 0.25$

(B) $0 < K_c < 0.25$

(C) 0.25 < K_c < 0.5

(D) $K_0 > 0.5$

Answer: (D)

Exp_e
$$G(s) = \frac{k_a G_p}{1 + k_a G_a}$$

characteristic equation 1+k G = 0

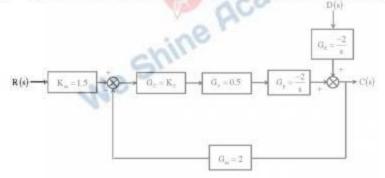
$$1+k_a, \frac{2}{s-1}=(s-1)+2k_a=0$$

$$s+(2k_{-1})=0$$

for stable closed loop response

$$\Rightarrow k > 0.5 \Rightarrow (D)$$
.

53. Consider the following block diagram for a closed-loop feedback control system



A proportional controller is being used with $K_c = -4$. If a step change in disturbance of magnitude 2 affects the system, then the value of the offset is

Answer: 0.49 to 0.51

$$\mathbf{Exp}, \qquad \frac{\mathbf{C(s)}}{\mathbf{D(s)}} = \frac{-2/s}{1 + 2k_{a} \cdot 0.5 \left(\frac{-2}{5}\right)} = \frac{-2/s}{1 - \frac{2k_{a}}{s}} = \frac{-2}{s - 2k_{a}}$$

$$D(s) = \frac{2}{s}$$

offset =
$$0 - \lim_{s \to 0} s C(s) = -\lim_{s \to 0} s \frac{2}{s} \left(\frac{-2}{s - 2k} \right) = \frac{4}{8} = 0.50$$

54. Determine the correctness or otherwise of the following Assertion [a] and Reason [r].

Assertion: Significant combustion of coke takes place only if it is heated at higher

temperature in presence of air.

Reason: C+O, $\rightarrow CO$, is an exothermic reaction.

(A) Both [a] and [r] are true and [r] is the correct reason for [a]

(B) Both [a] and [r] are true but [r] is not the correct reason for [a]

(C) [a] is correct but [r] is false
(D) Both [a] and [r] are false

Answer (B)

Exp. Both [a] and [r] are true but [r] is not the correct reason for [a].

55. Match the raw materials of Groups 1 and 2 with the final products of Group 3

Group 1	Group 2	Group 3
P ₁ : Ethylene	Q ₁ : Ammonia	R: Synthetic fibre
P ₁ : Propylene	Q ₂ : 1-Butene	R ₂ : Nylon 66
P _i : Adipie acid	Q ₅ : Ethylene glycol	R ₃ : LLDPE
Pa: Terephthalic acid	Q4: Hexamethylene diamine_	R. Acrylonitrile

(A)
$$P_1 + Q_2 \rightarrow R_3$$
; $P_2 + Q_1 \rightarrow R_4$; $P_3 + Q_4 \rightarrow R_2$; $P_4 + Q_4 \rightarrow R_4$

(B)
$$P_1 + Q_1 \rightarrow R_2$$
; $P_2 + Q_2 \rightarrow R_1$; $P_2 + Q_4 \rightarrow R_4$; $P_4 + Q_5 \rightarrow R_2$

(C)
$$P_1 + Q_2 \rightarrow R_2$$
; $P_2 + Q_3 \rightarrow R_3$; $P_3 + Q_4 \rightarrow R_3$; $P_4 + Q_1 \rightarrow R_3$

(D)
$$P_1 + Q_1 \rightarrow R_4$$
; $P_2 + Q_3 \rightarrow R_3$; $P_3 + Q_4 \rightarrow R_5$; $P_4 + Q_5 \rightarrow R_1$

Answer: (D)

Exp.

Raw material

w material

Product

tene

LLDPE (Linear low density PE)

Propylene + Ammonia

Adipic Acid + Hexomethylene diamine

Aerylonetrile Nylon – 66

Terephthalic acid + Ethylene glycol

Synthetic fibre